

Supplementary Information

AC-Induced Corrosion of Underground Steel Pipelines. Faradaic Rectification under Cathodic Protection: I. Theoretical Approach with Negligible Electrolyte Resistance

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List of Symbols

Alphabetic

$[O_2]_{\infty}$	Bulk concentration of dissolved oxygen	mol cm ⁻³
$[O_2]_{\text{int}}$	Interface concentration of dissolved oxygen	mol cm ⁻³
$\langle E_{\text{corr,AV}} \rangle$	Dimensionless corrosion potential shift; $= (E_{\text{corr,AV}} - E_{\text{corr,0}}) / \Delta E$	
$\langle I_{\text{corr,AV}} \rangle$	Dimensionless corrosion current; $= I_{\text{corr,AV}} / I_{\text{corr,0}}$	
B	Kinetic coefficient or Tafel constant ($= \pm \alpha n F / R T$)	V ⁻¹
C_d	Double layer capacitance	F cm ⁻²
CP	Cathodic protection	
D_{O_2}	Diffusion coefficient of dissolved oxygen	cm ² s ⁻¹
E	Potential at the interface	V
E_0	DC component of $E(t)$ corresponding to the CP potential	V
$E_{\text{corr,0}}$	Free corrosion potential or open circuit potential in absence of AC perturbation	V
F	Faraday ($= 96500$)	A s
f	Frequency of AC signal	Hz
I	Current density (+ for anodic and – for cathodic reaction)	A cm ⁻²
I_0	Corrosion current density under CP without AC signal	A cm ⁻²
$I_{B,k}$	Bessel function of k th order	
$I_{\text{corr,0}}$	So-called “free” corrosion current density	A cm ⁻²
I_{diff}	Diffusion component of the mixed kinetics	A cm ⁻²
I_F	Faradaic current	A cm ⁻²
K	Reaction rate constant	mol s ⁻¹
n	Number of electrons exchanged in anodic reaction	
R	Gas constant ($= 8.315$)	J mol ⁻¹ K ⁻¹
$r_{\text{diff,O}_2}$	Importance of the I_{diff} at $E_{\text{corr,0}}$; $-(1 - \lambda_{\text{H}_2\text{O}}) I_{\text{corr,0}} / I_{\text{lim,O}_2}$ at $E_{\text{corr,0}}$	
R_E	Electrolyte resistance	Ω cm ²
$r_{O_2/a}$	Ratio of Tafel constant ($-b_{c,O_2} / b_a$)	
R_p	Polarisation resistance	Ω cm ²
T	Absolute temperature	K
U	Overall potential between the reference and working electrodes	V

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Greek symbols

$\langle \Delta E \rangle$	Reduced amplitude of AC signal	
α	Transfer coefficient for tafelian process; between 0 and 1	
β	Tafel slope	V decade ⁻¹
δ	Thickness of Nernst diffusion layer	cm
ΔE	Peak voltage of AC perturbing interfacial signal	V
ΔU	Peak voltage of AC signal	V
$\lambda_{\text{H}_2\text{O}}$	Fraction of water reduction current at $E_{\text{corr},0}$; $I_{\text{corr},0,\text{H}_2\text{O}} / I_{\text{corr},0}$	
O_{O_2}	Flux of dissolved oxygen towards the electrode interface	mol s ⁻¹ cm ⁻²
ω	Angular frequency, pulsation ($= 2\pi f$)	rad s ⁻¹

Subscripts and suffixes

–	Mean value over one period of AC signal
a	Anodic reaction
c	Cathodic reaction
c,H ₂ O	Cathodic reaction of the water reduction reaction
c,O ₂	Cathodic reaction of the dissolved oxygen reduction reaction
corr,0	At the free corrosion without AC perturbation