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Chemometric Study of Perilla Fatty Acids from Subcritical n-Propane Extracted Oil

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O óleo de perilla (*Perilla frutescens*) foi extraído utilizando *n*-propano subcrítico e também pela metodologia oficial de Soxhlet, para efeito de comparação. Objetivou-se avaliar a influência dos fatores temperatura e pressão sobre a composição dos ácidos graxos (FA), através de um fatorial 2² completo em triplicata com ponto central. Ambos os fatores analisados contribuíram significativamente para o rendimento dos FA extraídos. As superfícies de resposta indicaram que o aumento da pressão e temperatura permitiu maior extração de ácidos graxos omega-3 e poli-insaturados (PUFA), e uma melhor razão entre PUFA e ácido graxos saturados (SFA). Através da função de desejabilidade, a melhor condição de extração com *n*-propano foi temperatura de 80 °C e pressão de 8 MPa. A análise multivariada distinguiu a condição ótima no grupo de maior conteúdo de PUFA, com destaque para o ácido alfa-linolênico, enquanto a metodologia de Soxhlet caracterizou-se com elevado teor de SFA.

Oil from perilla (*Perilla frutescens*) was extracted using subcritical *n*-propane and also the Soxhlet official methodology, for comparison. This work aimed at assessing the influence of the temperature and pressure factors on the composition of fatty acids (FA), using a full 2² factorial design in triplicate with central point. Both factors were significant for increasing the yield of extracted FA. The response surfaces showed that increasing pressure and temperature allowed the extraction of higher levels of n-3 and polyunsaturated fatty acids (PUFA) and greater ratio values of PUFA and saturated fatty acids (SFA). According to the desirability function, the best condition of extraction using *n*-propane was 80 °C for temperature and 8 MPa for pressure. In multivariate analysis the optimum condition was characterized by a higher content of PUFA, especially alphalinolenic fatty acid, while the Soxhlet methodology was characterized by high level of SFA.

Keywords: subcritical fluid extraction, fatty acids, *Perilla frutescens*, response surface methodology, principal component analysis

Introduction

Perilla (*Perilla frutescens* Linn, Britton) is a herbaceous plant native to Asia that belongs to the family Lamiaceae.¹ The grains are approximately 51% total lipids and 17% crude protein.² Perilla oil has a high content of polyunsaturated fatty acids, with 48-60% alpha-linolenic fatty acid (LNA, 18:3n-3) and 13-16% linoleic acid (LA, 18:2n-6).³ These fatty acids play important roles in metabolic processes. Through desaturase enzymes and elongases, they act in the production of other eicosanoid fatty acids from the omega-3 (n-3) and

omega-6 (n-6) series such as eicosapentaenoic acid (EPA, 20:5n-3), docosahexaenoic (DHA, 22:5n-3) and arachidonic acid (AA, 20:4n-6).⁴

Traditionally, methods of extracting vegetable oils employ organic solvents with high toxicity, which can cause environmental damage and harm the health of the population. Some techniques include high temperatures, favoring the degradation of thermolabile compounds.⁵ In this context, subcritical fluid extraction (SFE) is a promising technique to replace these methods. According to Lang and Wai,⁶ the main advantages of this method include the use of nontoxic solvents, relatively low operating temperature, greater selectivity and absence of solvent residues in the extract.

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SFE is characterized by the use of a solvent with intermediate properties between liquid and gas. Fluid characteristics, such as high density, diffusivity and low viscosity, provide it with an excellent solvating capacity. These characteristics may be controlled by the conditions of temperature and pressure, thereby improving the selectivity and solubility of compounds.^{7,8} Some researchers have investigated the application of experimental design in the optimization of this process. This application allows assessing the influence of factors on the expected response and defines the optimum condition.⁹⁻¹³

Carbon dioxide (CO_2) is the most widely used solvent and its extraction time can vary from 330 to 1380 minutes; however studies indicate that n-propane offers greater solvating power, which results in faster extraction in 40-85 min and the oil extracted has the same fatty acid profile when compared to CO_2 extraction.^{5,14-17}

The objective of this study was to extract lipids from perilla using *n*-propane as a solvent in the subcritical state, assess the influence of the factors temperature and pressure on the composition of the fatty acids in the total lipids by chemometric methods, and compare the results obtained to the official Soxhlet method.

Experimental

Sample preparation

Three batches of 5 kg of perilla grains were purchased in the local market of Maringá-PR, Brazil. The grains were ground in a Wiley mill to obtain a fine flour that was sieved, using the fraction that passed through a 14 mesh Tyler series sieve (WSTyler, USA). Later, the sample was homogenized and vacuum packed in polyethylene bags and frozen at –18 °C.

Experimental design

A full 2^2 factorial design in triplicate with center point was applied to investigate the influence of the factors temperature and pressure in the subcritical extraction on the composition of fatty acids, as shown in Table 1. These factors were chosen in accordance with studies reported in

Table 1. Factors and levels investigated in the experimental design for subcritical extraction with *n*-propane

Г.	T I 14	Cl1	Th	Level			
Factor	Unit	Symbol	Type -	-1	0	1	
Temperature	°C	Т	Numeric	40	60	80	
Pressure	MPa	P	Numeric	8	12	16	

the literature which have evaluated the extraction of lipids from oilseeds using subcritical *n*-propane as solvent at constant flow.¹⁵⁻¹⁷ The responses analyzed were the yields of saturated fatty acids (SFA), monounsaturated fatty acids (MUFA), polyunsaturated fatty acids (PUFA) and the ratios PUFA/SFA and n-6/n-3.

Procedure for subcritical fluid extraction

The experiments were performed in a laboratory-scale unit, as described by Souza *et al.*, 18 using *n*-propane (White Martins, 99.5% purity) as solvent. For each extraction the extraction column was filled with 25.0 g of ground and sieved perilla grains. The solvent flow rate was constant at $1.0 \text{ cm}^3 \text{ min}^{-1}$. Total lipids were extracted and collected at regular time intervals of 10 min in a glass tube and the mass was determined gravimetrically. The total time of each extraction was 90 min. The extraction yield was calculated as the percentage of the extracted oil mass divided by the mass of sample introduced into the extraction column.

Extraction of total lipids by the official method

Total lipids were extracted in a Soxhlet extractor (Nova Etica, Brazil). Approximately 4.0 g of ground and sieved perilla grains were extracted in a Soxhlet extractor using a mixture of ethyl ether-petroleum ether (1:1 v/v) as solvent, for 16 h at 65 °C in accordance with the procedure described by Instituto Adolf Lutz.¹⁹

Determination of fatty acids

The composition of fatty acids was determined by converting the total lipids into fatty acid methyl esters (FAME) according to the methylation method described by Hartman and Lago.²⁰ The FAME were separated in a CP-3380 gas chromatograph (Varian, USA) fitted with a flame ionization detector following the conditions used by Souza *et al.*.²¹

Retention times were compared to methyl ester standards (Sigma, USA). The methyl ester of tricosanoic acid was used as an internal standard for quantification of the fatty acids (Sigma, USA). The peak areas were determined with Star 5.0 software (Varian, USA). According to Joseph and Ackman²² (equation 1), correction factors for individual fatty acids (FA) in FAME with a flame ionization detector were used and their concentrations expressed in mg FA g⁻¹ of total lipids.

$$M_{x} = \frac{A_{X} \times Mp \times F_{CT}}{A_{P} \times M_{A} \times F_{CEA}} \tag{1}$$

where M_x is the mass of fatty acid X in mg g^{-1} of sample; Mp is the internal standard mass in mg; M_A is the sample mass in g; A_X is the area of fatty acid X; A_p is the internal standard area; F_{CT} is a theoretical correction factor; and F_{CEA} is the methyl ester correction factor for the fatty acid.

Indices of nutritional quality of the lipids

A better approach to the nutritional evaluation of fat is the utilization of indices based on the functional effects of fatty acid composition. These indices are available as the index of atherogenicity (IA) and index of thrombogenicity (IT) by Ulbricht and Southgate, ²³ as well as the hypocholesterolemic/hypercholesterolemic fatty acid ratio (HH) according to Santos-Silva *et al.*. ²⁴

Statistics and multivariate analyses

Initially, the results for individual fatty acids obtained from experimental conditions of subcritical extraction were subjected to analysis of variance (ANOVA). Subsequently, the values of the principal and interaction coefficients were calculated for the factorial design data. All variables had their normality and homogeneity of variance evaluated by residues. Then, analysis of variance (ANOVA between groups) was performed for all responses. Response surface methodology was applied to evaluate the coefficients of independent variables on the responses and establish the optimum region. The basic mathematical model used to fit the data was (equation 2):

$$\hat{Y}_i = b_0 + b_1 x_1 + b_2 x_2 + b_{12} x_1 x_2 \tag{2}$$

where \hat{Y}_i is the expected response, b_0 , b_1 , b_2 and b_{12} are the regression coefficients of the regression model and x_1 and x_2 are the levels of the independent variables.²⁵

With the models, the equations were arranged in a global response using a desirability function. The results obtained for the sums of polyunsaturated, monounsaturated and saturated fatty acids were used to estimate the global response. This procedure involved a transformation of each response (\hat{Y}_i) estimated for an individual value of desirability (d_i) , in which $0 \le d_i \le 1$, according to Derringer and Suich.²⁶

If the objective or target T to the response \hat{Y}_i is a maximum value, then equation 3 should be used.

$$d_{i} = \begin{cases} 0 & \hat{Y}_{i} < L \\ \frac{\hat{Y}_{i} - L}{T - L} \end{cases}^{r} \quad L \leq \hat{Y}_{i} \leq T \\ 1 & \hat{Y}_{i} > T \end{cases}$$

$$(3)$$

If the objective or target to the response \hat{Y}_i is a minimum value, then equation 4 should be used.

$$d_{i} = \begin{cases} 1 & \hat{Y}_{i} < T \\ \left(\frac{U - \hat{Y}_{i}}{U - T}\right)^{r} & T \leq \hat{Y}_{i} \leq U \\ 0 & \hat{Y}_{i} > U \end{cases}$$

$$(4)$$

where L and U are minimum and maximum limits, respectively.

The convenience function is linear when the weight r is equal to 1. If r > 1 there is more emphasis on targeting the closest value. Using 0 < r < 1 makes this less important.

Individual values of desirability (d_i) were arranged through a geometric average to form a global desirability value (D), which will attend to satisfy all response simultaneously. This single value of D [0,1] gives a global assessment of convenience and the arranged response levels, and D will increase at the same time that the properties balance becomes more favorable.

Principal component analysis (PCA) consisted of using the sums and ratios of fatty acids (loadings). For this analysis, the eighteen tests' averages were separated into groups (scores): A (tests 1 to 3), B (tests 4 to 6), C (tests 7 to 9), D (tests 10 to 12), E (tests 13 to 15), and F (Soxhlet, tests 16 to 18; n = 3). Averages were autoscaled, so that whole variables showed the same weight. In this way, PCA bidimensional graphics were obtained. All the statistical analyses were done using Statistica software version $8.0,^{27}$ adopting the 5% significance level for rejection of the null hypothesis (p < 0.05).

Results and Discussion

It was possible to quantify a total of six fatty acids, which were palmitic (16:0), stearic (18:0), oleic (18:1 n-9), linoleic (18:2 n-6), alpha-linolenic (18:3 n-3) and arachidic (20:0) acids. These results were similar to those found by other authors. ^{2,28,29} The difference in fatty acid composition may be influenced by edaphoclimatic, genetic and aging factors, conditions of extraction, and others. ³ Alphalinolenic acid was majoritarian in all the experiments, followed by oleic and linoleic acids. The sums and ratios of fatty acids are shown in Table 2.

The total lipid content extracted using subcritical fluid were 34.25, 35.01, 34.91, 34.78 and 34.88%, respectively, for tests A, B, C, D and E. The performance of subcritical extraction was described using kinetic curves (Figure 1), which were similar for all conditions. The extraction

Table 2. Quantification of sums and ratios of fatty acids extracted by subcritical fluid and the official method (Soxhlet) from perilla oil

Tests	Independent variables			Sums and ratios of fatty acids / (mg FA g ⁻¹ TL)							
	x ₁ / °C	x ₂ / MPa	SFA	MUFA	PUFA	n-6	n-3	PUFA/SFA	n-6/n-3		
1	1	1	82.77	173.60	669.03	141.98	527.05	8.08	0.27		
2	1	1	81.18	174.28	669.20	141.78	536.42	8.24	0.27		
3	1	1	80.00	169.81	675.02	138.21	527.82	8.44	0.26		
4	1	-1	82.87	180.88	660.89	143.91	516.98	7.97	0.28		
5	1	-1	83.68	179.62	660.83	146.00	514.83	7.89	0.28		
6	1	-1	83.28	180.25	660.86	144.96	515.9	7.93	0.28		
7	-1	-1	91.30	195.80	637.79	152.26	485.53	6.98	0.31		
8	-1	-1	90.54	198.46	636.02	152.42	483.60	7.02	0.31		
9	-1	-1	85.97	190.11	649.18	151.37	497.81	7.55	0.30		
10	-1	1	79.21	171.57	674.54	133.39	541.20	8.52	0.25		
11	-1	1	81.44	174.32	668.84	140.97	527.87	8.21	0.27		
12	-1	1	82.20	175.73	667.23	141.78	525.45	8.12	0.27		
13	0	0	83.32	179.10	662.27	145.39	516.88	7.95	0.28		
14	0	0	83.08	180.92	661.25	146.20	515.06	7.96	0.28		
15	0	0	81.04	175.12	671.55	142.22	529.33	8.27	0.27		
16	Soxhlet		93.11	181.46	650.40	147.64	502.76	6.98	0.29		
17	Sox	xhlet	94.76	180.80	649.66	147.62	502.04	6.85	0.29		
18	Sox	khlet	97.27	193.12	633.38	155.97	477.72	6.51	0.33		

FA: fatty acids; TL: total lipids; x_1 : temperature; x_2 : pressure; SFA: total saturated fatty acids; MUFA: total monounsaturated fatty acids; PUFA: total polyunsaturated fatty acids; n-6: total fatty acids from the omega-6 series; n-3: total fatty acids from the omega-3 series; PUFA/SFA: ratio between polyunsaturated and saturated fatty acids; n-6/n-3: ratio between fatty acids from the omega-6 and omega-3 series.

rate was higher in the first 50 min, and then there was a stabilization of yields.

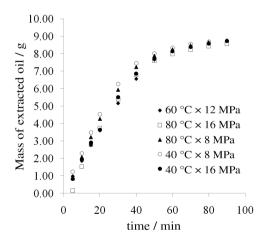


Figure 1. Kinetic curves of extraction using subcritical *n*-propane.

The total lipid content of perilla by the Soxhlet method was 40.46%; this content may be due to the extraction of other non-lipid compounds that are soluble in the mixture of ethyl ether and petroleum ether used in this extraction.^{30,31}

The regression coefficients for each one of the models, their confidence interval and coefficients of determination (R²) are shown in Table 3. Values of R² close to 1 indicate a good correlation between experimental and predicted data.³² Pagamunici *et al.*³³ found coefficients of determination of 0.85 for instrumental data *vs.* sensory analysis as a function of time and the models were well fitted. In this study, the values were greater than 0.80, which means that the linear model explained more than 80% of the data variability. The residual plots for each response showed normality, and homogeneity of variance was explained satisfactorily.

The limits of confidence intervals for the first-order term (x_1) in the sum of n-6 fatty acid series showed values with opposite signs (Table 3). All values are possible within a confidence interval, therefore it is possible that this value is zero. This fact demonstrates that there was a linear correlation between the variables, so there is no statistical evidence to keep this term in the model. Nevertheless, its permanence was preferred to preserve the mathematical hierarchy.³⁴

According to Table 3, the interaction coefficients for fatty acids from the n-3 series, PUFA and the PUFA/SFA ratio were negative, however data show that increased levels of principal coefficients contributed to improve the yield of these fatty acids.

Table 3. Regression coefficient, confidence interval and coefficients of determination of the responses applied to the response surface methodology

	Parameter									
	SFA	MUFA	PUFA	n-6	n-3	PUFA/SFA	n-6/n-3			
Mean	83.45	179.97	661.63	144.19	517.45	7.94	0.28			
	(82.48, 84.43) ^a	(178.39, 181.55) ^a	(658.86, 664.41) ^a	(142.42, 145.56) ^a	(513.69, 521.20) ^a	(7.82, 8.06) ^a	$(0.27, 0.28)^a$			
\mathbf{X}_1	-1.40	-3.96	5.18	-1.28	6.46	0.18	-5.8×10^{-3}			
	$(-2.49, -0.32)^a$	$(-5.73, -2.19)^a$	$(2.08, 8.29)^a$	$(-2.81, 0.25)^a$	(2.26, 10.66) ^a	$(0.05, 0.31)^a$	$(-0.01, -1.63 \times 10^{-3})^a$			
\mathbf{x}_2	-2.57	-7.15	9.86	-4.40	14.26	0.35	-0.01			
	$(-3.66, -1.47)^a$	$(-8.91, -5.38)^a$	$(6.75, 12.96)^a$	$(-5,93,-2.87)^a$	(10.06, 18.46) ^a	$(0.22, 0.49)^a$	$(-0.02, -9.96 \times 10^{-3})^a$			
x_1x_2	1.59	3.30	-4.74	2.25	-7.00	-0.19	7.50×10^{-3}			
	$(0.49, 2.68)^a$	$(1.54, 5.07)^a$	$(-7.84, -1.64)^a$	$(0.72, 3.78)^a$	(-11.19, -2.80) ^a	$(-0.33, -0.06)^a$	$(3.29 \times 10^{-3}, 0.01)^a$			
\mathbb{R}^2	0.805	0.917	0.870	0.829	0.880	0.832	0.879			

^aConfidence interval of coefficients at 95% confidence; x₁: temperature; x₂: pressure; R²: coefficient of determination; SFA: total saturated fatty acids; MUFA: total monounsaturated fatty acids; PUFA: total polyunsaturated fatty acids; n-6: total fatty acids from the omega-6 series; n-3: total fatty acids from the omega-3 series; PUFA/SFA: ratio between polyunsaturated and saturated fatty acids; n-6/n-3: ratio between fatty acids from the omega-6 and omega-3 series.

Tables 4 and 5 showed the results obtained by ANOVA for each factor studied in the model response. The pressure factor influenced the increased levels of n-6 series fatty acids, MUFA and the PUFA/SFA ratio the most, with contributions of 61.65, 60.27 and 53.71%, respectively (Table 4).

The values of F-test (Table 5) demonstrate the significance of regression coefficients and lack of fit. In general, if the calculated F value exceeds the tabulated F value, the term is considered significant at the defined level of confidence.³⁵ The interaction coefficient for the n-6 series fatty acids response was significant statistically, while the main coefficient of

Table 4. Results of ANOVA, sum of squares of the responses obtained in full 22 factorial design in triplicate with central point

Source -	Sum of squares										
	DF	SFA	MUFA	PUFA	n-6	n-3	PUFA/SFA	n-6/n-3			
X ₁	1	23.74	188.42	322.71	19.63	501.04	0.38	4.08×10^{-4}			
\mathbf{x}_2	1	79.26	613.61	1166.04	232.41	2441.31	1.52	2.41×10^{-3}			
$x_1 x_2$	1	30.34	131.27	270.27	60.79	588.00	0.45	6.75×10^{-4}			
Residual	11	32.38	84.83	262.29	64.15	480.145	0.48	4.82×10^{-4}			
Lack of fit	1	3.59	9.49	43.09	0.64	33.18	0.05	1.50×10^{-5}			
Pure error	10	28.78	75.34	219.2	63.51	446.96	0.42	$4.67\times10^{\text{-4}}$			
Total SS	14	165.72	1018.14	2021.33	376.99	4010.49	2.83	3.97×10^{-2}			

 x_1 : temperature; x_2 : pressure; SS: sum of squares; DF: degree of freedom; SFA: total saturated fatty acids; MUFA: total monounsaturated fatty acids; PUFA: total polyunsaturated fatty acids; n-6: total fatty acids from the omega-6 series; n-3: total fatty acids from the omega-3 series; PUFA/SFA: ratio between polyunsaturated and saturated fatty acids; n-6/n-3: ratio between fatty acids from the omega-3 series.

Table 5. Results of ANOVA, F-test and the responses obtained for the full 22 factorial design in triplicate with central point

G.	F-test									
Source	DF	SFA	MUFA	PUFA	n-6	n-3	PUFA/SFA	n-6/n-3		
\mathbf{x}_1	1	8.25	25.01	14.72	3.09	11.21	9.06	8.75		
\mathbf{X}_2	1	27.53	81.45	53.19	36.59	54.62	35.75	51.61		
$\mathbf{x}_1 \mathbf{x}_2$	1	10.54	17.43	12.33	9.57	13.15	10.64	14.46		
Lack of fit	1	1.25	1.26	1.97	0.10	0.74	1.23	0.32		
Residual	11									
Pure error	10									

 $\begin{aligned} &Ftab_{95\%,\ regression/residual\ (1,11)} = 4.84 \\ &Ftab_{95\%,\ lack\ of\ fit/pure\ error\ (1,10)} = 4.96 \end{aligned}$

 x_1 : temperature; x_2 : pressure; Ftab: tabulated F value; SFA: total saturated fatty acids; MUFA: total monounsaturated fatty acids; PUFA: total polyunsaturated fatty acids; n-6: total fatty acids from the omega-6 series; n-3: total fatty acids from the omega-3 series; PUFA/SFA: ratio between polyunsaturated and saturated fatty acids; n-6/n-3: ratio between fatty acids from the omega-6 and omega-3 series.

temperature was not significant. The yield of these fatty acids depended on the contribution of the coefficients: pressure (61.65%), interaction (16.13%) and temperature (5.21%), in this order (Table 4), and the greatest result was found at 40 °C and 8 MPa. These effects can be noted in the response surface models (Figure 2). The lack of fit of the models were not significant compared to the pure error.

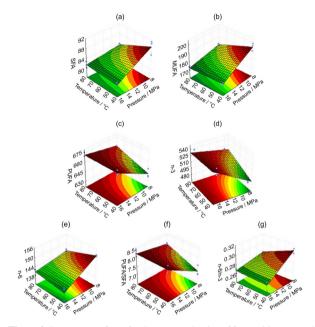


Figure 2. Response surfaces for the sums and ratios of fatty acids extracted by subcritical fluid extraction. (a) SFA: total saturated fatty acids; (b) MUFA: total monounsaturated fatty acids; (c) PUFA: total polyunsaturated fatty acids; (d) total fatty acids from the omega-3 series; (e) total fatty acids from the omega-6 series; (f) ratio between polyunsaturated and saturated fatty acids; (g) ratio between fatty acids from the omega-6 and omega-3 series.

The extraction by the official Soxhlet method showed a high yield of SFA, while the concentration of n-3 fatty acids was low. This indicates that the heating used during extraction in this method may have contributed to the degradation of the n-3 fatty acids, as these are more prone to hydrolysis, oxidation and polymerization at high temperatures.⁴

Principal component analysis (PCA, Figure 3) showed the distribution of three distinct groups. Principal component 1 (PC 1) explained 58.29% of data variance, and loadings indicated that n-3 fatty acids, total PUFA and the PUFA/SFA ratio were responsible for the formation of group 1. This was due to higher values of these items in experiments A, B, D and E. These effects can be noted in the response surface models (Figures 2c, d and f).

In PC 2 there was a negative contribution by SFA in the lower left quadrant, causing the separation of group 3 (Figure 3). The high contribution of MUFA to the left upper quadrant promoted the separation of group 2 due

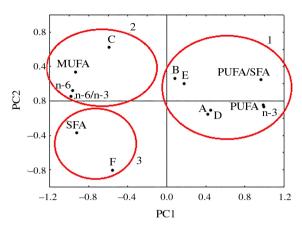


Figure 3. Principal component analysis of the fatty acid composition. PC: principal component; A: experiments 1 to 3; B: experiments 4 to 6; C: experiments 7 to 9; D: experiments 10 to 12; E: experiments 13 to 15; F: experiments 16 to 18 (Soxhlet).

to the greater concentration of this sum in the subcritical condition of 40 °C and 8 MPa (Figure 3, condition C). This principal component was responsible for 11.71% of the data variance.

Figure 4a shows the desirability function for the following restrictions: maximum value of total PUFA and MUFA: minimum value of total SFA. The maximum convenience achieved was 0.54 which corresponds to 83.03, 179.85 and 661.71 mg g⁻¹ of total lipids for SFA, MUFA e PUFA, respectively (Figure 4b). The highest level of temperature and low level of pressure were described as a point of major desirability (condition B) in favor of the process of extraction by subcritical fluids using *n*-propane. This result corroborates the separation of condition B in the group with the highest content of PUFA fatty acids, especially alpha-linolenic acid, by PC 1 (Figure 3). Figure 4b provides the response surface for the optimal region. The optimal extraction conditions of perilla oil (Figure 4) allowed us to obtain atherogenicity and thrombogenicity indexes equal to 0.08 and 0.05, respectively, and the HH ratio was 13.32. On the other hand, the official method presented IA: 0.08, IT: 0.06 and HH: 11.89, and did not compromise the quality of the oil. These indexes and ratios are important from a nutritional standpoint; in addition, lower IA and IT with higher HH values may attenuate the risk of cardiovascular diseases. 23,24,36 The incorporation of perilla oil in food processing seems to be promising, just like the use of flaxseed oil.21,33,37-39

Conclusions

The factorial design showed that the temperature and pressure factors were significant for the yield of fatty acids. All regression models were highly significant and the lack of fit was not significant. The response surfaces indicated that increased pressure and temperature allowed more n-3

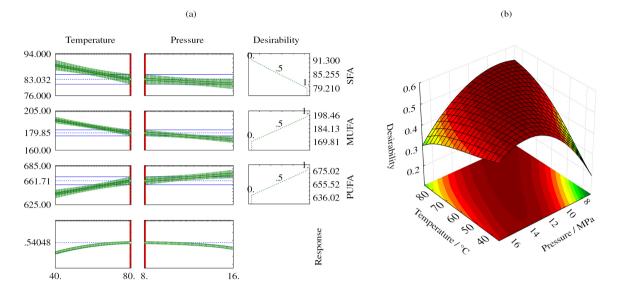


Figure 4. (a) Conditions of restriction and responses of the desirability function in the optimization of the extraction conditions using subcritical fluid and a full 2^2 design in triplicate with a central point; (b) response surfaces for the optimal region through the applied desirability functions.

fatty acids and PUFA to be extracted and a better PUFA/SFA ratio to be obtained. The main effect of the temperature was not significant for n-6 and this was due to the high significance of the interaction effect. PC 1 distinguished the conditions A, B, D and E due to the high contribution by the loadings: n-3 fatty acids, PUFA and PUFA/SFA. The desirability function that allowed us to determine the best conditions of lipid extraction with subcritical *n*-propane were 80 °C and 8 MPa. Multivariate analysis characterized this extraction condition in the group with the highest content of PUFA, especially alpha-linolenic fatty acid.

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References

- 1. Nitta, M.; Lee, J. K.; Ohnishi, O.; Econ. Bot. 2003, 57, 245.
- Longvah, T.; Deosthale, Y. G.; J. Am. Oil Chem. Soc. 1991, 68, 781.
- 3. Lee, D. S.; Noh, B. S.; Bae, S. Y.; Kim, K.; *Anal. Chim. Acta.* **1998**, *358*, 163.
- Martin, C. A.; Almeida, V. V.; Ruiz, M. R.; Visentainer, J. E. L.; Matsushita, M.; Souza, N. E.; Visentainer, J. V.; Rev. Nutr. 2006, 19, 761.
- 5. Reverchon, E.; de Marco, I.; *J. Supercrit. Fluids.* **2006**, *38*, 146.
- 6. Lang, Q.; Wai, C. M.; Talanta 2001, 53, 771.

- 7. Temelli, F.; J. Supercrit. Fluids 2009, 47, 583.
- 8. Passos, C. P.; Silva, R. M.; Silva, F. S.; Coimbra, M. A.; *Chem. Eng. J.* **2010**, *160*, 634.
- Follegati-Romero, L. A.; Piantino, C. R.; Grimaldi, R.; Cabral,
 F. A.; J. Supercrit. Fluids 2009, 49, 323.
- Nyam, K. L.; Tan, C. P.; Lai, O. M.; Long, K.; Che Man, Y. B.; Food Bioprod. Process 2010, 88, 239.
- Leitão, N. C. M. C. S.; Prado, G. H. C.; Veggi, P. C.; Meireles, M. A. A.; Pereira, C. G.; J. Supercrit. Fluids 2013, 78, 114.
- Santos, O. V.; Correa, N. C. F.; Carvalho Jr., R. N.; Costa,
 C. G. F.; Lannes, S. C. S.; *J. Food Eng.* 2013, 117, 499.
- 13. Ruttarattanamongkol, K.; Siebenhandl-Ehn, S.; Schreiner, M.; Petrasch, A. M.; *Ind. Crops Prod.* **2014**, *58*, 68.
- Garcia, V. A. S.; Silva, C.; Filho, L. C.; Acta Sci., Technol. 2013, 35, 499.
- 15. Corso, M. P.; Fagundes-Klen, M. R.; Silva, E. A.; Filho, C. L.; Santos, J. N.; Freitas, L. S.; Dariva, C.; *J. Supercrit. Fluids* **2010**, *52*, 56.
- Nimet, G.; da Silva, E. A.; Palu, F.; Dariva, C.; Freitas, L. S.;
 Neto, A. M.; Filho, L. C.; *Chem. Eng. J.* 2011, *168*, 262.
- Pederssetti, M. M.; Palu, F.; da Silva, E. A.; Rohling, J. H.;
 Cardozo-Filho, L.; Dariva, C.; *J. Food Eng.* **2011**, *102*, 189.
- Souza, A. T.; Benazzi, T. L.; Grings, M. B.; Cabral, V.; da Silva, E. A.; Cardozo-Filho, L.; Antunes, O. A. C.; *J. Supercrit. Fluids* 2008, 47, 182.
- Instituto Adolfo Lutz; Métodos Químicos e Físicos para Análise de Alimentos, 5ª ed.; Imesp: São Paulo, 2005.
- 20. Hartman, L.; Lago, R. C. A.; Lab. Pract. 1973, 22, 475.
- 21. Souza, A. H. P.; Gohara, A. K.; Rodrigues, A. C.; Souza, N. E.; Visentainer, J. V.; Matsushita, M.; *Acta Sci., Technol.* **2013**, *35*, 757.
- 22. Joseph, J. D.; Ackman, R.; J. Am. Oil Chem. Soc. 1992, 75, 488.
- 23. Ulbricht, T. L. V.; Southgate, D. A. T.; Lancet 1991, 338, 985.

- Santos-Silva, J.; Bessa, R. J. B.; Santos-Silva, F.; *Livest. Prod. Sci.* 2002, 77, 187.
- Granato, D.; Bigaski, J.; Castro, I. A.; Masson, M. L.; Food Chem. 2010, 121, 899.
- 26. Derringer, G.; Suich, R.; J. Qual. Technol. 1980, 12, 214.
- 27. StatSoft, Inc.; *Statistica: Data Analysis Software System, version* 8.0; StatSoft: Tulsa, 2007.
- 28. Kim, H. K.; Choi, H.; Life Sci. 2005, 77, 1293.
- 29. Kim, J. K.; Park, S. Y.; Na, J. K.; Seong, E. O.; Yu, C. Y.; *J. Agric. Food Chem.* **2012**, *60*, 2257.
- Su, C. H.; Fu, C. C.; Chang, Y. C.; Nair, G. R.; Ye, J. L.; Chu,
 I. M.; Wu, W. T.; Biotechnol. Bioeng. 2008, 99, 1034.
- Brum, A. A. S.; Arruda, L. F.; Regitano-d'Arce, M. A. B.; *Quim. Nova* 2009, *32*, 849.
- 32. Pujari, V.; Chandra, T. S.; Process Biochem. 2000, 36, 31.
- Pagamunici, L. M.; Souza, A. H. P.; Gohara, A. K.; Silvestre,
 A. A. F.; Visentainer, J. V.; Souza, N. E.; Gomes, S. T. M.;
 Matsushita, M.; Cienc. Tecnol. Aliment. 2014, 34, 127.

- 34. Neto, B. B.; Scarminio, I. S.; Bruns, R. E.; *Como Fazer Experimentos: Pesquisa e Desenvolvimento na Ciência e Indústria*, 2ª ed.; Editora da Unicamp: Campinas, 2001.
- 35. Teófilo, R. F.; Ferreira, M. M. C.; Quim. Nova 2006, 29, 338.
- 36. Ratnayake, W. M.; Galli, C.; Ann. Nutr. Metab. 2009, 55, 8.
- Pagamunici, L. M.; Gohara, A. K.; Souza, A. H. P.; Bittencourt,
 P. R. S.; Torquato, A. S.; Batiston, W. P.; Gomes, S. T. M.; Souza,
 N. E.; Visentainer, J. V.; Matsushita, M.; J. Braz. Chem. Soc.
 2014, 25, 219.
- Souza, A. H. P.; Gohara, A. K.; Pagamunici, L. M.; Visentainer,
 J. V.; Souza, N. E.; Matsushita, M.; Acta Sci., Technol. 2014,
 36, 157.
- Fuchs, R. H. B.; Ribeiro, R. P.; Matsushita, M.; Tanamati,
 A. A. C.; Bona, E.; Souza, A. H. P.; LWT--Food Sci. Technol.
 2013, 54, 440.

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